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# Full Length Article

# Dynamic fluid interactions during CO<sub>2</sub>-ECBM and CO<sub>2</sub> sequestration in coal seams. Part 2: CO<sub>2</sub>-H<sub>2</sub>O wettability



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#### ABSTRACT

In addition to CO<sub>2</sub>-CH<sub>4</sub> interactions (Part 1), the success of CO<sub>2</sub> enhanced coalbed methane (CO<sub>2</sub>-ECBM) and geological sequestration are significantly affected by the CO2-H2O wettability. Wettability controls both gas desorption and transport and is influenced by injection pressure, reservoir temperature and the state of water that is present – as either adsorbed- or free-water. Dynamic changes in wettability remains poorly constrained – due to the innate difficulty and invasive nature of conventional measurements (e.g., captive gas bubble and pendent drop tilted plate methods). In part 2, we use nuclear magnetic resonance (NMR) as a non-invasive method to explore the mechanisms of these factors (pressure, temperature, water-state) on CO<sub>2</sub>-H<sub>2</sub>O wettability during CO2-ECBM. Results for contrasting subbituminous coal and anthracite show that the CO2 wettability of coals significantly increases with increasing CO2 injection pressure up to 5 MPa before stabilizing to a limiting value. This suggests that the most economically-suitable injection pressure is ~5 MPa. CO<sub>2</sub> wettability also increases with a decrease in temperature suggesting that shallower reservoirs may be marginally improved in this trend. Additionally, the presence of non-adsorbed water in coals significantly reduces both the sensitivity of CO<sub>2</sub> wettability to pressure and the absolute magnitude of wettability relative to the case where free-water is absent. Thus, draining free-water from the reservoir will serve the dual purposes of both increasing gas transport and the potential for desorption from the perspective of CO<sub>2</sub>-H<sub>2</sub>O wettability. The far-reaching results in this study, together with the companion paper (Part 1) are significant for evaluating CO<sub>2</sub>-ECBM improvement both in enhancing methane recovery and CO2 utilization in coals.

#### 1. Introduction

Industrial emissions of  $CO_2$  are of sufficient magnitude that they represent an important factor in modifying climate, promoting sea level rise and posing a serious threat to biodiversity and humankind [1–3]. Total global  $CO_2$  emissions rose to  $\sim\!37$  billion tons in 2018 and if continued at this pace will contribute to a global average temperature increase of  $\sim\!3.5$  °C and sea level rise of  $\sim\!15$ –95 cm by the end of the century [4–6].  $CO_2$  sequestration in geological formations is a potential mitigation strategy with long-term storage in abandoned hydrocarbon reservoirs, deep saline aquifers, the ocean and coal seams [7–10]. Of these methods,  $CO_2$  injection into coal reservoirs not only has great potential for the geological sequestration of  $CO_2$  but also offers the benefit of enhancing methane recovery.

Conventional methods of coalbed methane (CBM) recovery are by reservoir depressurization to enhance gas production [11,12].

Production enhancement techniques include hydraulic fracturing and gas injection (e.g., CO2, N2) technique. Hydraulic fracturing techniques mainly use high-pressure fluid injection, typically water, to create and connect fractures, successfully improving Chinese CBM production over the past few decades [13-15]. However, the presence of liquidous water in fractures/macropores may promote a sharp decline in methane production as a result of water blocking [16,17]. Alternatively, the sorption capacity of CO2 in coals is ~2-10 times that of methane [18,19], establishing CO<sub>2</sub> injection into coal reservoirs as a feasible method to enhance methane recovery. This has been implemented in the field, based on the mechanism of competitive adsorption between CH<sub>4</sub> and CO<sub>2</sub> [20,21]. In April 2010, 233.6 t of CO<sub>2</sub> was injected into well SX-001in the Qinshui Basin, resulting in a 2.5-fold increase in the post-injection methane production rate [22]. The estimated CO<sub>2</sub> sequestration capacity in the global unminable coal reserve could reach ~200 Gt [23], demonstrating the significant potential of CO<sub>2</sub> enhanced

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Fig. 1. Deep-Well core samples used in this study (a, subbituminous coal, 712 m, Southern Junngar Basin; b, anthracite coal, 557 m, Southern Qinshui Basin).

coalbed methane ( $CO_2$ -ECBM) recovery for the complimentary sequestration of  $CO_2$ .

Considering the presence of water in coal reservoirs, wettability in coal- $H_2O$ - $CO_2$  mixtures is a fundamental factor controlling the interrelations among capillary pressure,  $CO_2$  adsorption and fluid invasion mechanisms. This directly influences the rate of methane recovery and  $CO_2$  geological sequestration capacity [24,25]. The most commonly used methods to characterize  $CO_2$ - $H_2O$  wettability in coals are the captive gas bubble and pendent drop tilted plate methods [26–28]. The  $CO_2$  gas bubble contact angle is positively correlated with injection pressure: a higher gas pressure is indicative of a greater  $CO_2$  wettability [26]. The water contact angles measured by the pendent drop tilted plate method exhibit a positive relationship with  $CO_2$  injection pressure, whereas negative related to experimental temperature [28]. However, enough time is much-required for  $CO_2$  to sorb on coal surface, but the measurement needs to be performed quickly for these methods, that may result inaccurate of  $CO_2$ - $H_2O$  wettability.

Water may exist in three states at typical in-situ coal reservoir conditions. This is as: (1) Adsorbed water, physically adsorbed to the microporous surface. (2) Capillary water, confined in the small pore capillaries. (3) Free water, saturating the macro-pores or fractures and distant from a gas-water interface [29-31]. The presence of adsorbed water directly decreases methane adsorption capacity, with free water potentially limiting gas access to the coal interior via water blocking and the Jamin effect [32]. During CO<sub>2</sub>-ECBM, the injected CO<sub>2</sub> can exist as an adsorbed phase on the surface of the coal matrix, as a free phase in fractures and also dissolved within the interstitial water [33] - similar to the methane occurrences in coals. Nevertheless, the impact of the presence of multiphase water on CO2 wettability, and its impact on CO<sub>2</sub>-ECBM remain unresolved. This is due both to the reality that CO<sub>2</sub>-ECBM is a new and evolving technique, but also since the challenges of non-invasive measurement of this response under in-situ conditions are particularly challenging. Non-invasive monitoring of this response is one approach that can yield high fidelity measurements and resolve this issue.

Nuclear magnetic resonance (NMR) is widely used to evaluate the petrophysical properties of hydrogen-bearing reservoir fluids (i.e., water and methane) [34–39]. Exist researches have proved that NMR measurement could serve as an accurate method to investigate the  $\rm CO_2/$ 

CH<sub>4</sub> interactions during CO<sub>2</sub>-enhanced gas recovery (CO<sub>2</sub>-EGR) process [40-44]. Xu et al. [40] found that the internal pore connectivity and methane migration pathway of coals were enhanced after CO2 injection. Liu et al. [33] suggested that the methane sweep efficiency can achieve ~80% by injection of CO<sub>2</sub> in shale reservoir. Compared against measurements made by standard USBM or Amott index experiments, the geometric mean of the NMR transverse relaxation time  $(T_2)$  has been demonstrated as an accurate index to probe water wettability in conventional reservoirs (e.g., sandstones and carbonates) [45-47]. For a typical coal NMR spectrum, the change in the rightmost peak of the  $T_2$ distribution provides a quantitative characterization of water wettability either with or without CO2 injection [48]. However, prior studies have been limited to water-wetting of coal powder and neglect consideration of the influence of different water states on CO2 wettability. In addition, the sensitivity of sortie mass and sorption rates to CO2 wettability, and the impact of pressure and temperature are illdefined - and present a unique opportunity for NMR as an exploration tool. The following explores the dynamic interaction between CO2 and H<sub>2</sub>O during staged CO<sub>2</sub>-ECBM flooding at in situ reservoir. In particular, the response of subbituminous coal and anthracite are followed for variable injection pressures, temperatures and water occurrence states by using NMR. The effect of these conditions on wettability is vital in guiding CO2-ECBM in recovery for both enhanced gas recovery (EGR) and for CO<sub>2</sub> geological sequestration.

#### 2. Samples and experimental methods

# 2.1. Properties of samples

The experimental samples including subbituminous coal and subbituminous coal that were cored from exploration wells in the Southern Junngar Basin and Southern Qinshui Basin, respectively (Fig. 1). The sampling depth of the subbituminous coal is 712 m (Table 1), with an in-situ reservoir pressure of 4.2 MPa [49]; while that of the anthracite coal is 557 m, with an in-situ reservoir pressure of 3.5 MPa [49]. The maximum vitrinite reflectance ( $R_{\rm o,m}$ ) of the subbituminous coal is 0.54%, with 76.5% vitrinite content and 21.7% inertinite content. The Anthracite is characterized by high vitrinite maceral composition (87.9%), with an  $R_{\rm o,m}$  of 3.16% (Table 1). Contact angle was measured

**Table 1**Basic petrophysical characteristics of the selected coal samples (from the companion paper [49]).

Sample	Coal basin	R <sub>o,m</sub> (%)	Depth (m)	Contact angle (°)	Maceral co	Maceral composition (%)		
					V	I	E	М
Subbituminous Anthracite	Southern Junngar Southern Qinshui	0.54 3.16	712 557	67.5 107.6	76.5 87.9	21.7 9.2	1.1 2.1	0.7 0.8

Notes:  $R_{o,m}$  is maximum vitrinite reflectance, V- vitrinite; I- inertinite; E- exinite; M- minerals.

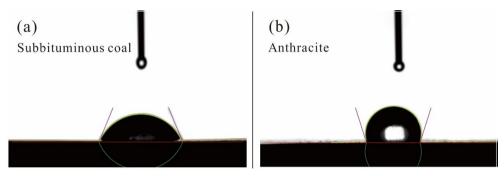


Fig. 2. Photographs of the contact angle measurement.

on the high-pressure compressed artificial surface of the disc, as noted in Fig. 2 and listed in Table 1. The subbituminous coal is water-wetting, with a contact angle of 67.5°, whereas the anthracite water-non-wetting, with a contact angle of 107.6°.

#### 2.2. Low-field NMR

Low-field NMR methods are widely used to evaluate the petrophysical properties of hydrogen-bearing reservoir fluids (i.e., water and methane) including the evolution of fluid typing, methane adsorption capacity, and wettability 35–39,[45–50]. The transverse relaxation time  $(T_2)$  is a preferable index parameter, relative to longitudinal relaxation time  $(T_1)$  – due to its fast and convenient application in NMR laboratory testing. According to the principle of low-field NMR, the hydrogen nuclei  $(^1H)$  in the reservoir fluids characterized by  $T_2$  are affected by the bulk relaxation time  $(T_{2B})$ , surface relaxation time  $(T_{2S})$  and diffuse relaxation time  $(T_{2D})$ . This is expressed as following [51–53]:

$$\frac{1}{T_2} = \frac{1}{T_{2B}} + \frac{1}{T_{2S}} + \frac{1}{T_{2D}} = \frac{3T_k}{298\eta} + \rho_2 \left(\frac{S}{V}\right) + \frac{D(\gamma G T_E)^2}{12}$$
(1)

where  $T_k$  is the laboratory temperature, K;  $\eta$  represents fluid viscosity, cp;  $\rho_2$  represents surface relaxivity,  $\mu$ m/ms; S represents pore specific surface, um²; V represents pore volume, um³, D represents molecular diffusion coefficient, um²/ms,  $\gamma$  represents proton gyromagnetic ratio, MHz/T; G represents field-strength gradient, Gs/cm; and  $T_E$  represents echo spacing time, ms. Typically, by applying a low-homogenous magnetic field intensity and the Carr-Purcell-Meiboom-Gill (CPMG) sequence, the parameters  $1/T_{2B}$  and  $1/T_{2D}$  in Eq. (1) can be neglected. Thus, Eq. (1) can be simply expressed as:

$$\frac{1}{T_2} = \frac{1}{T_{2S}} = \rho_2 \left(\frac{S}{V}\right) = F_S \left(\frac{\rho_2}{r}\right) \tag{2}$$

where  $F_{\rm S}$  is the pore shape factor; and r is the pore size,  $\mu \rm m$ . As seen in Eq. (2),  $T_2$  is positive correlated with the pore size – a longer  $T_2$  represents a lager pore size. The occurrence of water in different forms is apparent in the NMR spectrum as the left peak for adsorbed water ( $T_2 < 10$  ms), the central peak for capillary water (10 ms  $< T_2 < 100$  ms) and the right peak for free water (100 ms  $< T_2$ ) [32,35].

#### 2.3. Experimental set-up and procedures

Fig. 3 shows a schematic diagram of the experimental set-up. It comprises five components: (1) a gas supply system for two different gases (He and CO<sub>2</sub>) contained in cylinders and with a booster pump; (2) a gas exhaust system – used for waste gas recovery; (3) a sample cell system, including a thermostat (to maintain a designated experimental temperature) and a non-magnetic PEEK cell (to hold the coal samples); (4) a reference cell, designed to transport and sustain methane for the sample cell; and (5) a MiniMR-60 NMR measurement device.

Prior to all experiments, the air tightness is measured and any contaminating impurities are removed by injecting He gas into experimental set-up. The coals were powdered to 60–80 mesh (size of 0.18–0.25 mm) then dried at 374.15 K for 12 h to remove the internal moisture. To explore the effect of pressure, temperature, and water occurrence on  $\rm CO_2\text{-}H_2O$  wettability during the  $\rm CO_2\text{-}ECBM$  process, we performed three separate experimental series: A, B and C (Table 2). There procedures were:

Experimental Series A: a) Place 10 g of dried coal powder into a canister of oversaturated- $K_2SO_4$  solution, leave to reach an equilibrium water saturation before placing into the sample cell and vacuuming for 3 h. b) Set and maintain the temperature at 298 K for the full experimental series A. c) Inject  $CO_2$  into reference cell at 6 MPa and open valve G8 (Fig. 3) to fill the sample cell with  $CO_2$  to a pressure of 3 MPa. d) Measure the sample cell  $T_2$  spectrum every 60 min until the difference between subsequent measurements is negligible. e) Increase the  $CO_2$  pressure in the sample cell and repeat the experimental procedure (d) at each of four incremented pressures of 4, 5, 6 and 7 MPa.

The experimental procedures of Experimental Series B and C were identical to Series A, except for experimental conditions in Series B (different temperatures of 308, 318 and 328 K but at a constant  $CO_2$  pressure of 5 MPa), and the different sample preparation in Series C (5 g of free water was added after the equilibrium water condition). For the Experimental Series B, the sample cell temperature was controlled and maintained by the temperature sensor (Fig. 3), that can be set to any temperature in the range of 298–333 K. In this study, the NMR measurement was performed using Suzhou Niumag MiniMR-60 analytical instrument, with a low constant magnetic field of 0.5 T. The parameters were set as 0.3 ms echo spacing, 6000 ms waiting time, and 10,000 echo numbers, same as companion paper [49].

# 3. Results and discussion

#### 3.1. Quantitative NMR model for water

To characterize the  $\rm CO_2\text{-}H_2O$  wettability of coals, it is necessary to establish a quantitative model for water based on the NMR data. Fig. 4a shows the NMR  $T_2$  distributions for different masses of free water – a clear peak with long relaxation time is apparent at 200–1000 ms. The NMR total amplitude shows a linearly relationship with water mass (Fig. 4b), that can be expressed as:

$$M_{water} = 0.0001A \quad (R^2 = 0.9933)$$
 (3)

where  $M_{water}$  is the mass of water, g; and A is the NMR  $T_2$  amplitude, dimensionless.

#### 3.2. Effect of pressure on CO<sub>2</sub>-H<sub>2</sub>O wettability

As shown in Fig. 5, at equilibrium water content, the powdered coal sample contains only adsorbed water (black line with open circles) – as indicated by the fast relaxation time at  $\sim$ 0.1–2 ms – this is a result of

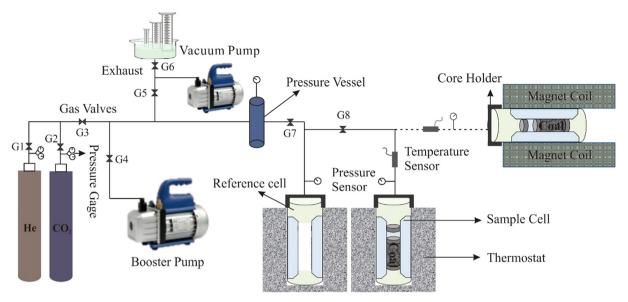


Fig. 3. Schematic diagram of the experimental set-up (modified from the companion paper [49]).

**Table 2** Experimental series and sample preparation.

Experimental series	Sample preparation	Temperature (K)	CO <sub>2</sub> pressure (MPa)
A	Equilibrium water condition	298	3, 4, 5, 6, and 7
В	Equilibrium water condition	308, 318, and 328	5
С	Added 5 g free water after equilibrium water	298	3, 4, 5, 6 and 7

the diffusion behavior of the evaporated water molecules. The amplitude of the  $T_2$  peak for the subbituminous coal is much larger than that for anthracite for the equilibrium water content experiments, per unit mass of coal powder. The main reason for this is that the subbituminous coal has a higher water wettability than anthracite (Fig. 2), enabling more evaporated water to adsorb into micropores.

 $CO_2$  injection pressure is a critical parameter defining improvement in methane recovery – higher injection pressures drive higher methane sweep efficiency. To assess the effect of pressure on  $CO_2$ -H<sub>2</sub>O wettability during the progress of  $CO_2$ -ECBM, Experimental Series A was performed under five different pressures (3, 4, 5, 6 and 7 MPa) but at a constant temperature of 298 K.

Fig. 5 shows the real-time dynamic changes in the NMR  $T_2$  distributions following  $CO_2$  injection at 3 MPa in Experimental Series A.

With the injection of CO<sub>2</sub>, the NMR spectrum changes from single-peaked to triple-peaked. The clear P1 peak ( $T_2=0.01$ –6 ms), with a fast relaxation time, indicates the characteristics of adsorbed water in micropores. The in-conspicuous P2 peak ( $T_2=10$ –30 ms) corresponds to the water in the small capillaries. The P3 peak ( $T_2>100$  ms), with high  $T_2$  relaxation times, references the free water in the sample. Considering the important distribution of adsorbed water to wettability, to simplify the interpretation, we used the P1 peak to represent the adsorbed water, the P2 and P3 peak to represent the non-adsorbed water.

In Experiment Series A, the coal powder at equilibrium water content was flooded by  $CO_2$  at 3 MPa with an NMR measurement performed every 1 h. As shown in Fig. 5, with an increase in the  $CO_2$  exposure time, the adsorbed water  $T_2$  amplitude decreases (P1 peak) and

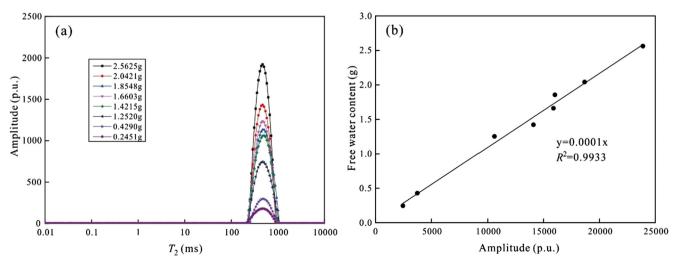
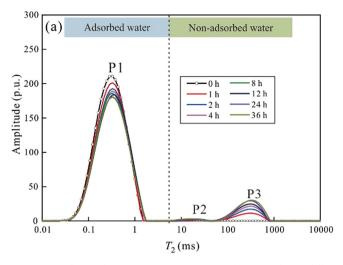


Fig. 4. NMR T<sub>2</sub> distributions for different masses of water (a) and relationship between the NMR T<sub>2</sub> amplitude relative to water mass (b).



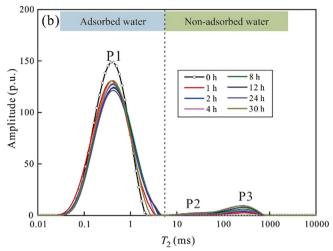


Fig. 5. Changes in NMR T2 spectrum of water with time following CO2 injection at 3 MPa (a, subbituminous coal; b, anthracite).

the non-adsorbed water amplitude increases significantly (P3 peak). Since the system is closed, this suggests the transformation of adsorbed water into non-adsorbed water as a result of  $\mathrm{CO}_2$  injection. It should be noted that the P3 peak gradually shifts rightward over time – indicating that the free water spreads to larger pores.

The geometric mean of the  $T_2$  relaxation time ( $T_{\rm 2gm}$ ) is an accurate index to probe water wettability in porous media (e.g., sandstones, carbonates and coals) [45–48]. The geometric mean is defined as:

$$T_{\text{2gm}} = \exp\left[\sum \frac{\ln(T_{2i})A_i}{A_{total}}\right] \tag{4}$$

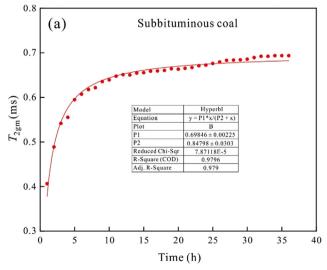
where  $T_{2\rm i}$  are the individual values of  $T_2$ , ms;  $A_{\rm i}$  their amplitude at  $T_{2\rm i}$ , dimensionless; and  $A_{\rm total}$  is the total amplitude of the NMR spectrum, dimensionless. Generally, a reduction in the  $T_{\rm 2gm}$  value represents the movement of fluid into smaller pores – an indication of a weaker water wettability [45,46].

Fig. 6 shows the real-time dynamic changes in  $T_{\rm 2gm}$  resulting from CO<sub>2</sub> flooding at 3 MPa for both subbituminous coal (Fig. 6a) and anthracite (Fig. 6b). During the CO<sub>2</sub> soaking process (3 MPa), the subbituminous coal reestablished an equilibrium in CO<sub>2</sub>-H<sub>2</sub>O interaction after ~36 h where the  $T_{\rm 2gm}$  increases from 0.41 ms to 0.69 ms. Equilibrium in  $T_{\rm 2gm}$  is reestablished for anthracite after ~30 h where  $T_{\rm 2gm}$  increases from 0.36 ms to 0.65 ms. Again, these results suggest that the adsorbed water spreads into the larger pores – due to the decrease in

water wettability in coals following  $CO_2$  injection. During this process,  $T_{\rm 2gm}$  first increases rapidly before asymptote to an ultimate value, similar in form a Langmuir-like sorption isotherm.

As shown in Fig. 7, the adsorbed water (P1 peak) amplitude decreases significantly with an increase in  $CO_2$  injection pressure, whereas the non-adsorbed water (P2 and P3 peak) amplitude increases. In order to exclude the effect of evaporative water loss, we compared the change in relative water mass rather than absolute water mass in quantifying water migration – i.e., its exchange from adsorbed to non-adsorbed state following an increase in  $CO_2$  pressure (Fig. 8). The relative mass of adsorbed water for the subbituminous coal fell from 100% to 65% as  $CO_2$  pressure increased from 0 MPa to 7 MPa, liberating  $\sim$ 35% of the originally adsorbed water to the non-adsorbed state. For the anthracite, the increase in relative mass of non-adsorbed water was both smaller and slower, rising from 0% to 19% as  $CO_2$  pressure was raised to 7 MPa. The reduction in relative mass of adsorbed water (i.e., increase in mass of non-adsorbed water) during the  $CO_2$ -H<sub>2</sub>O interaction, represents a transformation from water-wet to  $CO_2$ -wet during the  $CO_2$ -ECBM process.

In increasing  $CO_2$  pressure from 0 to 7 MPa, the  $T_{\rm 2gm}$  increases from 0.39 ms to 1.79 ms for subbituminous coal, and 0.36 ms to 1.12 ms for anthracite (Fig. 9). This suggests the reduction in water wettability and growth in  $CO_2$  wettability with pressure – consistent with prior observations on coals [26,48]. This change in wettability may result from



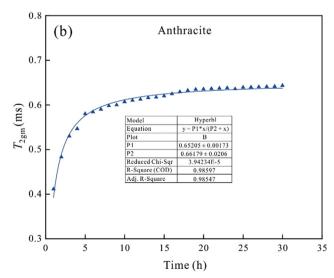
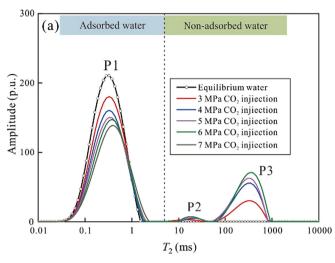


Fig. 6. Changes in  $T_{2gm}$  as a function of time for  $CO_2$  present at 3 MPa for (a) subbituminous coal and (b) anthracite.



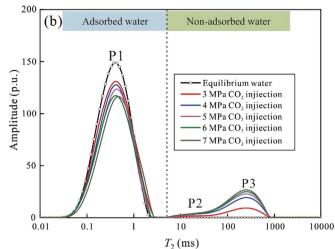


Fig. 7. Changes in water  $T_2$  spectrum for different  $CO_2$  injection pressures (a, subbituminous coal; b, anthracite).

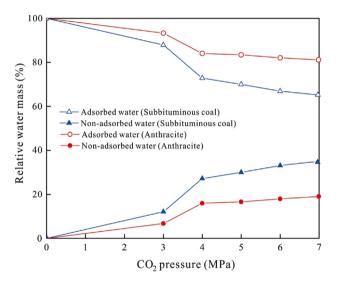


Fig. 8. Relative changes in water mass changes as a function of CO2 pressure.

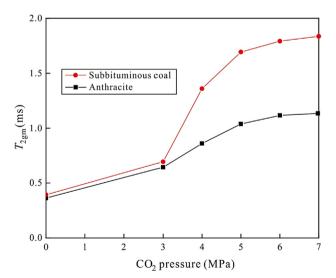


Fig. 9. Changes in  $T_{2gm}$  with  $CO_2$  injection pressure.

the increase in  $CO_2$  pressure due to a pressure induced: (1) increase the  $CO_2$  adsorption capacity of coals [54], (2) increase in dissolved  $CO_2$  content in water, resulting in an increase in  $H^+$  concentrations, which

further improves  $CO_2$  wettability [55], (3) increase in  $CO_2$  density, increasing the interfacial tension by strengthening the intermolecular attraction between both the  $CO_2$ - $H_2O$  and  $H_2O$ - $H_2O$  bonds [56].

The  $\rm H_2O$  wettability change with  $\rm CO_2$  injection pressure – the change is gradual below 3 MPa with a rapid rise from 3 to 5 MPa before stabilizing at ~7 MPa. For the subbituminous coal, the average net increase of  $T_{2gm}$  is 0.65 ms in the range 3–5 MPa, compared to only 0.07 ms above 5 MPa, per unit pressure of  $\rm CO_2$  injected. A similar trend in  $T_{2gm}$  as a function of  $\rm CO_2$  pressure is also found for anthracite, indicating only a minor increase in  $\rm CO_2$  wettability when  $\rm CO_2$  pressure is > 5 MPa.

#### 3.3. Effect of temperature on CO<sub>2</sub>-H<sub>2</sub>O wettability

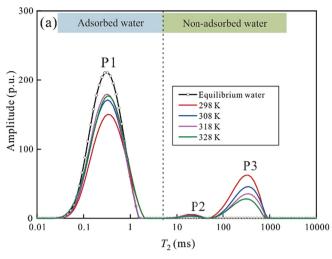
Fig. 10 shows the  $T_2$  spectra for both subbituminous coal and anthracite at temperatures of 298 K, 308 K, 318 K and 328 K, but at a fixed  $\rm CO_2$  pressure of 5 MPa (Experimental Series B). With increasing of temperature,  $T_2$  amplitude representing the adsorbed water increases and that for the non-adsorbed water declines. This indicates that increasing temperature increases the water wettability and correspondingly decreases the  $\rm CO_2$  wettability.

The change in relative mass of water, sequestered in either adsorbed or non-adsorbed state, is shown as a function of temperature in Fig. 11. When temperature rises from 298 K to 328 K in Experimental Series B (constant pressure), the relative mass of adsorbed water increased from 70% to 83% for subbituminous coal and increased from 83% to 94% for anthracite. As shown in Fig. 12, the  $T_{2gm}$  decreases with an increase in temperature for both subbituminous coal and anthracite. As temperature is raised to 328 K, the  $T_{2gm}$  falls from 1.69 ms to 0.65 ms for the subbituminous coal. For anthracite, the  $T_{2gm}$  decreases more slowly with temperature, falling from 1.04 ms to 0.55 ms. The variation with temperature of both  $T_{2gm}$  and the relative mass of adsorbed/non-adsorbed water both indicate the decrease in  $CO_2$  wettability with increasing temperature in coals.

Two principal factors may be responsible for this  $CO_2$  wettability decrease with increasing temperature. First,  $CO_2$  adsorption capacity is known to gradually decrease with an increase in temperature – due to the increase in kinetic energy and rate of diffusion of  $CO_2$  [48]. Second, the intermolecular attractive forces between in  $CO_2$ -H<sub>2</sub>O and H<sub>2</sub>O-H<sub>2</sub>O decrease with rising temperature, and result in the reduction of  $CO_2$ -H<sub>2</sub>O surface tension [56].

# 3.4. Effect of water content on CO<sub>2</sub>-H<sub>2</sub>O wettability

The form of water occurrence (adsorbed versus non-adsorbed) on



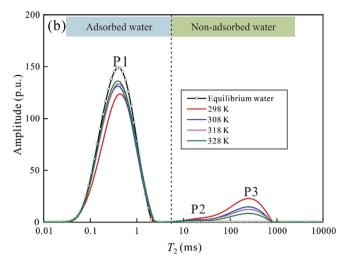


Fig. 10. Changes in water  $T_2$  spectrum with temperature (a, subbituminous coal; b, anthracite).

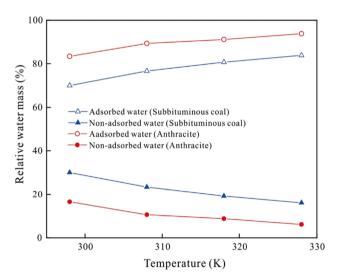


Fig. 11. Changes in relative water mass with temperature for  ${\rm CO_2}$  injection at 5 MPa.

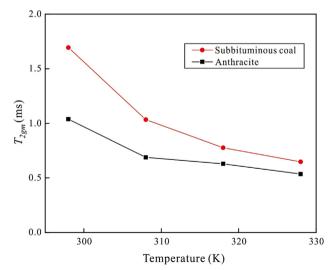


Fig. 12. Changes in  $T_{2gm}$  with temperature for  $CO_2$  injection at 5 MPa.

potential impacts CO2-H2O wettability for both subbituminous coal and anthracite. As shown in Fig. 5, when the coal contains only adsorbed water in the initial equilibrium water condition, the  $T_2$  distribution is unimodal with the only of P1 peak. After addition of free water in the coal sample, the  $T_2$  distribution changes to multiple peaks that represents both the adsorbed water and added non-adsorbed free water (Fig. 13). Changes in the water  $T_2$  spectra with injection pressure  $CO_2$ are shown in Fig. 13 (Experimental Series C). Similar to the variations for the equilibrium water content condition (Experimental Series A), the adsorbed water  $T_2$  amplitude decreases and non-adsorbed amplitude increases with increased pressure for both two coals. The features of the change in adsorbed water mass with pressure (Experimental Series C) are clarified in Fig. 14a. At the conclusion of the Experimental Series C, the adsorbed water content falls from 0.32 g to 0.24 g for the subbituminous coal and from 0.31 g to 0.19 g for the anthracite. This indicates the transformation of adsorbed water into non-adsorbed states. Again, two different CO2-H2O wettability change rates are apparent after raising CO<sub>2</sub> pressure: an initial rapid increase at < 5 MPa followed by stabilization (Fig. 14b), similar to the changes in where no free water is present (Experimental Series A), at least in terms of the  $T_{2gm}$  proxy.

 ${\rm CO_2 ext{-}H_2O}$  wettability is typically presumed to be a fixed physical parameter for a typical coal sample, regardless of whether it is treated under equilibrium water condition or with free water added. Thus, to investigate the influence of the various phase of water occurrence on  ${\rm CO_2 ext{-}H_2O}$  wettability of coals, we use the normalized  $T_{2gm}$  rather than absolute  $T_{2gm}$ . As shown in Fig. 15, for both subbituminous coal and anthracite, the normalized  $T_{2gm}$  increases significantly with an increase in pressure both for equilibrium water (Experimental Series A) and free water added conditions (Experimental Series C). This indicates that  ${\rm CO_2}$  injection pressure has fixed impact in decreasing water wettability with pressure independent of the form of water that is present. However, this impact on wettability is much reduced in the presence of free water (Fig. 15). The principal reason is likely that the non-adsorbed water occupies pore throat and renders these sorption sites unavailable for  ${\rm CO_2}$ .

# 3.5. Potential applications of this study

This study has used a novel NMR relaxation method to probe changes in  $CO_2$ - $H_2O$  wettability that result from  $CO_2$  flooding, as an analog to  $CO_2$ -ECBM. The experimental observations suggest that  $CO_2$ - $H_2O$  wettability of coals, are mainly affected by injection pressure, reservoir temperature and the state of water occurrence.

Experimental observations revealed that the sorption capacity of

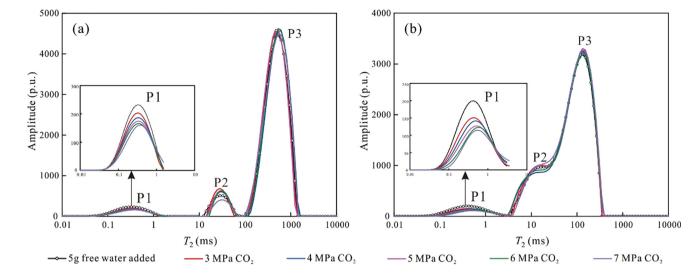


Fig. 13. Changes in water  $T_2$  spectrum with increasing  $CO_2$  injection pressure -5 g free water added after equilibrium water condition is reached (a, subbituminous coal; b, anthracite).

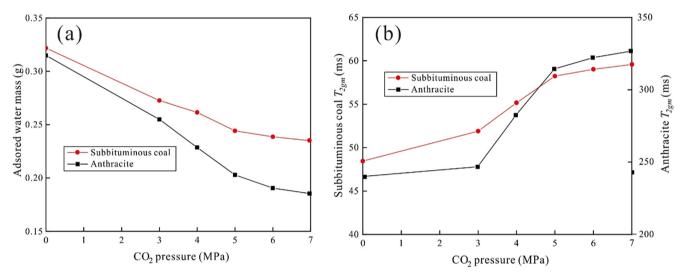


Fig. 14. Changes in adsorbed water amplitude (a) and  $T_{2gm}$  (b) with  $CO_2$  injection pressure.

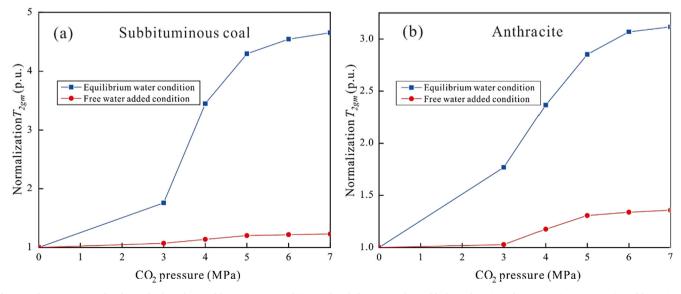


Fig. 15. Change in normalized  $T_{2gm}$  both at the equilibrium water condition and with free water then added as a function of  $CO_2$  injection pressure (a, subbituminous coal; b, anthracite).

 $CO_2$  is ~2-10 times that of methane in coals [21,22]. The injection of CO2 into coal reservoirs, both in laboratory and field experiments, has been successful in enhancing methane recovery. As discussed in Sections 3.2 and 3.4, increasing the injection pressure increases the CO2 wettability in coals with and without the presence of free water. However, a higher injection pressure often corresponds to a greater economic expense. Considering the rate change in wettability with pressure either absent (Experimental Series A) or with free water (Experimental Series C), the optimal injection pressure suggested in this study is ~5 MPa for elevating methane recovery. This is because wettability changes little above the pressure and therefore there is little increase in methane recovery even for an increased injection cost. The CO<sub>2</sub> wettability of coals declines with the increasing temperature (Experimental Series B), indicating that lower temperature is more suitable in enhancing methane recovery from the perspective of wettability in coals. Thus, shallower and cooler seams would be more productive, from this standpoint. But this remains a parameter - changing the temperature - that would be intractable to change for a coalbed reservoir.

In current field applications, the presence of large quantalities of water in fractures/macropores usually inhibits and sometimes largely eliminates methane production – the water blocking problem – present both in hydraulic fracturing and for  $\rm CO_2\text{-}ECBM$ . As discussed in Section 3.4, the presence of non-adsorbed water reduces the sensitivity of  $\rm CO_2$  wettability to pressure, potentially resulting in a reduction in CBM production. Thus, it is necessary to drain the free water, overcoming the negative impacts of non-adsorbed water in improving the  $\rm CO_2$  wettability, further enhancing the production rate of CBM.

In addition to enhancing methane recovery, injecting  $CO_2$  into coal reservoirs also has a potentially significant impact in  $CO_2$  geological sequestration and storage.  $CO_2$  sequestration and storage in coal reservoirs are primarily influenced by the  $CO_2$  adsorption capacity [24,48]. Since increasing  $CO_2$  wettability in coals increases  $CO_2$  adsorption capacity – this will further increase the potential mass of  $CO_2$  sequestered and stored. Regardless of the different modes of water occurrences in coals, adsorbed versus free, elevated pressures and low temperatures favor increased mass of  $CO_2$  sequestered.

#### 4. Conclusion

We evaluated the effect of  $CO_2$  injection pressure and temperature, together with different states of occurrence of water (adsorbed- versus free-water) on  $CO_2$ -H $_2O$  wettability of subbituminous coal and anthracite using NMR. Conclusions are drawn as follows:

- (1) The principal forms of water in coals are as: adsorbed water (P1 peak,  $T_2 < 6$  ms); and non-adsorbed water (including P2 peak and P3 peak,  $T_2 > 6$  ms). Coal powder under an equilibrium water state contains only adsorbed water. Conversely, any subsequently added water contributes a non-adsorbed phase that supplement the pre-existing adsorbed phase in the micro-pores.
- (2) CO<sub>2</sub> wettability of coals increases with an increasing in the CO<sub>2</sub> injection pressure. This change in CO<sub>2</sub> wettability increases with increase in pressure to < 5 MPa before stabilizing at an asymptotic maximum magnitude. Absent a significant increase in wettability above 5 MPa suggest the optimal injection pressure is 5 MPa for both enhancing methane recovery and CO<sub>2</sub> sequestration from the single perspective of wettability.
- (3) CO<sub>2</sub> wettability increases with a decrease in temperature and thus sequestered mass will be increased in lower-temperature coal reservoirs, all other factors being equal. Thus, shallow seams would benefit from this behavior, although changing reservoir temperature to benefit from this response is unlikely viable.
- (4) The presence of non-adsorbed water in coals significant decreases the rate of change in CO<sub>2</sub> wettability with pressure and reduces the maximum magnitude of the impact at elevated temperature. Thus,

the presence of free-water further results in the reduction in CBM production as a result of desorption, in addition to any impacts due to the occluding of pore and fractures and impeding transport. Thus, water drainage to improve methane transport in a dewatered pore/fracture network will additively aid in increasing the potential for methane drainage and CO<sub>2</sub> storage.

#### CRediT authorship contribution statement

Sijian Zheng: Validation, Writing - original draft, Investigation. Yanbin Yao: Conceptualization, Methodology, Supervision, Writing - review & editing, Project administration, Funding acquisition. Derek Elsworth: Writing - review & editing, Validation. Dameng Liu: Resources. Yidong Cai: Visualization.

## **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supplementary data

Supplementary data to this article can be found online at https://doi.org/10.1016/j.fuel.2020.118560.

# References

- Liu YY, Wilcox J. Molecular simulation studies of CO<sub>2</sub> adsorption by carbon model compounds for carbon capture and sequestration applications. Environ Sci Technol 2013;47:95–101.
- [2] Sarkodie SA, Strezov V. Effect of foreign direct investments, economic development and energy consumption on greenhouse gas emissions in developing countries. Sci Total Environ 2019;646:862–71.
- [3] Yan H, Zhang JX, Zhou N, Li M. Staged numerical simulations of supercritical CO<sub>2</sub> fracturing of coal seams based on the extended finite element method. J Nat Gas Sci Eng 2019;65:275–83.
- [4] Meng M, Qiu ZS, Zhong RZ, Liu ZG, Liu YF, Chen PJ. Adsorption characteristics of supercritical CO<sub>2</sub>/CH<sub>4</sub> on different types of coal and a machine learning approach. Chem Eng J 2019;368:847–64.
- [5] Mcinnes KL, White CJ, Haigh ID, Hemer MA, Hoeke RK, Holbrook NJ, et al. Natural hazards in Australia: sea level and coastal extremes. Clim. Chang. 2016;139:69–83.
- [6] Yan H, Zhang JX, Rahman SS, Zhou N, Suo Y. Predicting permeability changes with injecting CO<sub>2</sub> in coal seams during CO<sub>2</sub> geological sequestration: A comparative study among six SVM-based hybrid models. Sci Total Environ 2020;705:135941.
- [7] Elliot TR, Celia MA. Potential restrictions for CO<sub>2</sub> sequestration sites due to shale and tight gas production. Environ Sci Technol 2012;46(7):4223–7.
- [8] Verma MK. Fundamentals of Carbon Dioxide-Enhanced Oil Recovery (CO<sub>2</sub>-EOR). A Supporting Document of the Assessment Methodology for Hydrocarbon Recovery Using CO<sub>2</sub>-EOR Associated with Carbon Sequestration; U.S. Department of the Interior. U.S. Geological Survey 2015.
- [9] Bhattacharjee G, Kumar A, Sakpal T, Kumar R. Carbon dioxide sequestration: Influence of porous media on hydrate formation kinetics. ACS Sustainable Chem Eng 2015;3:1205-14.
- [10] Fan CJ, Elsworth D, Li S, Zhou LJ, Yang ZH, Song Y. Thermo-hydro-mechanical-chemical couplings controlling CH<sub>4</sub> production and CO<sub>2</sub> sequestration in enhanced coalbed methane recovery. Energy 2019;173:1054–77.
- [11] Ranathunga AS, Perera MSA, Ranjith PG, Wei CH. An experimental investigation of applicability of CO<sub>2</sub> enhanced coal bed methane recovery to low rank coal. Fuel 2017;189:391–9.
- [12] Zhang XG, Ranjith PG. Experimental investigation of effects of CO<sub>2</sub> injection on enhanced methane recovery in coal seam reservoirs. J. CO<sub>2</sub> Util. 2019;33:394–404.

- [13] Yao YB, Liu DM, Yan TT. Geological and hydrogeological controls on the accumulation of coalbed methane in the Weibei field, southeastern Ordos Basin. Int J Coal Geol 2014;121:148–59.
- [14] Yuan XH, Yao YB, Liu DM, Pan ZJ. Spontaneous imbibition in coal: Experimental and model analysis. J Nat Gas Sci Eng 2019;67:108–21.
- [15] Jia L, Li KW, Zhou JB, Yan ZM, Wang YW, Mahlalela BM. Experimental study on enhancing coal-bed methane production by wettability alteration to gas wetness. Fuel 2019:255:115860.
- [16] Fairhurst DL, Indriati S, Reynolds BW, Lewis JW, Holcomb MW, Starr FF. Advanced technology completion strategies for marginal tight gas sand reservoirs: a production optimization case study in south Texas. J Am Stat Assoc 2007;25:56–7.
- [17] Li X, Fu XH, Ranjith PG, Fang Y. Retained water content after nitrogen driving water on flooding saturated high volatile bituminous coal using low-field nuclear magnetic resonance. J Nat Gas Sci Eng 2018;57:189–202.
- [18] Wong S, Law D, Deng X, Robinson J, Kadatz B, Gunter WD, et al. Enhanced coalbed methane and CO<sub>2</sub> storage in anthracitic coals—microplots test at South Qinshui, Shanxi. China. Int. J. Greenh. Gas Control 2007;1:215–22.
- [19] Kedzior S. Accumulation of coal-bed methane in the south-west part of the Upper Silesian coal basin (southern Poland). Int J Coal Geol 2009;80:20–34.
- [20] Zhang XG, Ranjith PG, Perera MSA, Ranathunga AS, Zhang BN. Gas transportation and enhanced coalbed methane recovery processes in deep coal seams: a review. Energy Fuels 2016;30(11):8832–49.
- [21] Zhou YB, Li ZH, Zhang RL, Wang GZ, Yu H, Sun GZ, et al. CO<sub>2</sub> injection in coal: Advantages and influences of temperature and pressure. Fuel 2019;236:493–500.
- [22] Pan ZJ, Ye JP, Zhou FB, Tan YL, Connell LD, Fan JJ. CO<sub>2</sub> storage in coal to enhance coalbed methane recovery: a review of field experiments in China. Int Geol Rev 2018;60:754–76.
- [23] Mukherjee M, Misra S. A review of experimental research on Enhanced Coal Bed Methane (ECBM) recovery via CO<sub>2</sub> sequestration. Earth Sci Rev 2018;179:392–410.
- [24] Han F, Busch A, Wageningen N, Yang J, Liu Z, Krooss BM. Experimental study of gas and water transport processes in the inter-cleat (matrix) system of coal: anthracite from Qinshui Basin. China. Int. J. Coal Geol. 2010;81:128–38.
- [25] Zhu CJ, Wan JM, Tokunaga TK, Liu N, Lin BQ, Wu HR. Impact of CO<sub>2</sub> injection on wettability of coal at elevated pressure and temperature. Int. J. Greenh. Gas Control. 2019;91:102840.
- [26] Sakurovs R, Lavrencic S. Contact angles in CO<sub>2</sub>-water-coal systems at elevated pressures. Int J Coal Geol 2011:87:26–32.
- [27] Shojai KN, Rudolph ES, Wolf KH, Ashrafizadeh SN. Wettability determination by contact angle measurements: hvbB coal-water system with injection of synthetic flue gas and CO<sub>2</sub>. J Colloid Interface Sci 2011;364(1):237–47.
- [28] Arif M, Barifcani A, Lebedev M, Iglauer S. CO<sub>2</sub>-wettability of low to high rank coal seams: implications for carbon sequestration and enhanced methane recovery. Fuel 2016;181:680–9.
- [29] Allardice DJ, Evans DG. The-brown coal/water system: Part 2. Water sorption isotherms on bed-moist Yallourn brown coal. Fuel 1971;50:236–53.
- [30] Yao YB, Liu DM, Liu J. Assessing the water migration and permeability of large intact bituminous and anthracite coals using NMR relaxation spectrometry. Transp Porous Media 2015;107:527–42.
- [31] Shi JT, Chang YC, Wu SG. Development of material balance equations for coalbed methane reservoirs considering dewatering process, gas solubility, pore compressibility and matrix shrinkage. Int J Coal Geol 2018;195:200–16.
- [32] Wang F, Yao YB, Wen ZA, Sun QP, Yuan XH. Effect of water occurrences on methane adsorption capacity of coal: A comparison between bituminous coal and anthracite coal. Fuel 2020;266:117102.
- [33] Liu J, Xie LZ, Elsworth D, Gan Q. CO<sub>2</sub>/CH<sub>4</sub> competitive adsorption in shale: implications for enhancement in gas production and reduction in carbon emissions. Environ Sci Technol 2019;53:9328–36.

- [34] Timur A. Pulsed nuclear magnetic resonance studies of porosity, movable fluid, and permeability of sandstones. J Petrol Technol 1969;21:775–86.
- [35] Yao YB, Liu DM, Che Y, Tang DZ, Tang SH, Huang WH. Petrophysical characterization of coals by low-field nuclear magnetic resonance (NMR). Fuel 2010;89:1371–80.
- [36] Yao YB, Liu DM, Xie SB. Quantitative characterization of methane adsorption on coal using a low-field NMR relaxation method. Int J Coal Geol 2014;201:32–40.
- [37] Zhao YX, Zhu GP, Dong YH, Danesh NN, Chen ZW, Zhang T. Comparison of low-field NMR and microfocus X-ray computed tomography in fractal characterization of pores in artificial cores. Fuel 2017;210:217–26.
- [38] Zheng SJ, Yao YB, Liu DM, Cai YD, Liu Y. Characterizations of full-scale pore size distribution, porosity and permeability of coals: a novel methodology by nuclear magnetic resonance and fractal analysis theory. Int J Coal Geol 2018;196:148–58.
- [39] Shikhov I, Li RP, Arns CH. Relaxation and relaxation exchange NMR to characterise asphaltene adsorption and wettability dynamics in siliceous systems. Fuel 2018;220:692–705.
- [40] Xu JZ, Zhai C, Liu SM, Qin L, Wu SJ. Pore variation of three different metamorphic coals by multiple freezing-thawing cycles of liquid CO<sub>2</sub> injection for coalbed methane recovery. Fuel 2017;208:41–51.
- [41] Xu JZ, Zhai C, Liu SM, Qin L, Dong RW. Investigation of temperature effects from LCO<sub>2</sub> with different cycle parameters on the coal pore variation based on infrared thermal imagery and low-field nuclear magnetic resonance. Fuel 2018;215:528–40.
- [42] Liu J, Yao YB, Liu DM, Elsworth D. Experimental evaluation of CO<sub>2</sub> enhanced recovery of adsorbed-gas from shale. Int J Coal Geol 2017;179:211–8.
- [43] Liu J, Xie LZ, Yao YB, Gan Q, Zhao P, Du LH. Preliminary study of influence factors and estimation model of the enhanced gas recovery stimulated by carbon dioxide utilization in shale. ACS Sustainable Chem Eng 2019;7(24):20114–25.
- [44] Liu X, Zhang JZ, Bai YF, Zhang YP, Zhao Y, Cheng XY, et al. Pore structure petrophysical characterization of the Upper Cretaceous oil shale from the Songliao basin (NE China) using low-field NMR. J Spectrosc. 2020;:9067684.
- [45] Fleury M, Deflandre F. Quantitative evaluation of porous media wettability using NMR relaxometry. Magn. Reson. Imag. 2003;21(3–4):385–7.
- [46] Looyestijn W, Hofman J. Wettability-index determination by nuclear magnetic resonance. SPE Res. Eval. Eng. 2006;9(2):146–53.
- [47] Chen J, Hirasaki GJ, Flaum M. Effect of OBM on wettability and NMR responses. J. Petr. Sci. Eng. 2006;52:161–71.
- [48] Sun XX, Yao YB, Liu DM, Zhou Y. Investigations of CO<sub>2</sub>-water wettability of coal: NMR relaxation method. Int J Coal Geol 2018;188:38–50.
- [49] Zheng SJ, Yao YB, Elsworth D, Liu DM, Cai YD. Characterization of dynamic fluids interactions during CO<sub>2</sub>-ECBM and CO<sub>2</sub> sequestration in coal seams. Part 1: CO<sub>2</sub> – CH<sub>4</sub> interactions. Energy Fuels 2020. https://doi.org/10.1021/acs. energyfuels.0c01371.
- [50] Connolly PRJ, Vogt SJ, Iglauer S, May EF, Johns ML. Capillary trapping quantification in sandstones using NMR relaxometry. Water Resour Res 2017;53:7913–32.
- [51] Kleinberg RL, Horsfield MA. Transverse relaxation processes in porous sedimentary rock. J. Magn. Reson. 1990;88:9–19.
- [52] Coates GR, Xiao LZ, Primmer MGNMR. Logging Principles and Applications. Gulf. Publishing Company; 1999.
- [53] Guo R, Kantzas A. Assessing the water uptake of Alberta coal and the impact of CO<sub>2</sub> injection with low-field NMR. J Can Pet Technol 2009;48:40–6.
- [54] Busch A, Gensterblum Y. CBM and CO<sub>2</sub>-ECBM related sorption processes in coal: a review. Int J Coal Geol 2011;87:49–71.
- [55] Ibrahim AF, Nasr-El-Din HA. Effect of water salinity on coal wettability during CO<sub>2</sub> sequestration in coal seams. Energy Fuels 2016;30:7532–42.
- [56] Cho CH, Urquidi J, Singh S, Park SC, Robinson GW. Pressure effect on the density of water. J Phys Chem A 2002;106:7557–61.